

polymer communications

On the van Krevelen/Hoftyzer relationship for the high-temperature limiting viscosities of polymer melts

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The van Krevelen/Hoftyzer limiting viscosities $(T \rightarrow \infty)$ of polymer melts are often lower than the hightemperature viscosity of low-molecular weight liquids or the viscosity of air at 20°C and 1 bar. The origin of this surprising result is discussed. © 1997 Elsevier Science Ltd. All rights reserved.

(Keywords: polymer melts; limiting viscosity ($T \rightarrow \infty$); activation energy)

In refs 1 and 2, van Krevelen and Hoftyzer discussed the temperature dependence of the viscosity of polymer melts. Viscosity η_{cr} at the critical molecular weight (transition from M^{+1} to $M^{3,4}$ dependence) was plotted in the normalized Arrhenius diagram shown in Figure 1. At low temperatures (just above T_g) the line is curved and follows a Vogel/WLF course3; at high temperatures, the line is more or less straight suggesting true Arrhenius behaviour. Assuming such Arrhenius behaviour, the limiting flow-activation energy $E_{\eta}(\infty)$ and the limiting viscosity $\eta_{cr}(\infty)$ are determined as indicated.

According to the procedure of Figure 1, van Krevelen and Hoftyzer determined $E_n(\infty)$ and $\eta_{cr}(\infty)$ for various polymers. The data sources are given in ref. 1 and examples of viscosity vs temperature curves can be found in ref. 1 or in Fig. 15.3 of ref. 2. The resulting activation energies (from Table 15.5 of ref. 2) are reproduced in Table 1.

Interestingly, van Krevelen and Hoftyzer found an empirical correlation between the flow activation energy $E_n(\infty)$ and the limiting viscosity $\eta_{\rm cr}(\infty)$. It is given by equation (15.38) of ref. 2 reading

¹⁰log
$$\eta_{\rm cr}(\infty) = -1.4 - 0.085 E_n(\infty)$$
 (1)

with the viscosity in Pas and the activation energy in $kJ mol^{-1}$. The last column of *Table 1* gives the limiting viscosity $\eta_{cr}(\infty)$ as calculated with equation (1) from the activation energies given in Table 1. The remarkable *point* is that the limiting viscosity $\eta_{cr}(\infty)$ decreases with increasing activation energy and drops to values as low as 10^{-8} Pa s (see also Fig. 15.5 of ref. 2).

For non-associated and low-molecular weight liquids, the limiting viscosity $(T \rightarrow \infty)$ generally lies at about 10^{-4} Pa s⁴⁻⁶. Moreover, the viscosity of air at 20°C and 1 bar is 1.7×10^{-5} Pa s. Thus, the values of 10^{-5} - 10^{-8} Pas shown by *Table 1* are really surprising.

Figure 2 shows that van Krevelen's limiting viscosity decreases with increasing T_g . This is related to the decrease in $\eta_{\rm cr}(\infty)$ with increasing activation energy [equation (1)] since T_g roughly increases with the flow activation energy (see Table 1 and refs 7 and 8). Assuming that the limiting viscosity of polymers exceeds that of low-molecular weight liquids (10^{-4} Pa s) , we conclude from Figure 2 that van Krevelen's extrapola-

tions fail for polymers with a $T_g > 200$ K. A tentative explanation for this failure is given in Figure 3. As an example, we take rigid PVC. This material has a T_g of 81°C. The thermal stability of the polymer prevents viscosity measurements at temperatures far above 200°C. So, the viscosity is measured for $T_{g}/T > 0.70$, i.e. most probably in the curved part of the plots of Figures 1 and 3. This would lead to an activation energy (E_a) that is too high $[>E_n(\infty)]$ and a $\eta_{\rm cr}(\infty)$ -value that is too low (see extrapolated dashed line in Figure 3). In contrast, viscosities of low- $T_{\rm g}$ materials such a PE or PDMS can be measured at temperatures much further removed from T_g , i.e. at $T_{\rm g}/T$ values considerably lower than 0.70. For such materials, the linear (Arrhenius) part of the curve will be reached more easily and the activation energy as well as $\eta_{\rm cr}(\infty)$ will approach the correct values.

A semi-quantitative check of the idea is obtained by applying the WLF equation with the 'universal' constants $c_{1g} = 17$ and $c_{2g} = 51^{\circ}C^3$ (subscript g denotes that T_g was taken as reference temperature). For simplicity, we omit the Arrhenius term which is sometimes added for a better description at very high temperatures³; such omission hardly affects the results. We write the WLF equation in the Vogel form'

$$\ln \eta/\eta_{\infty}^* = B/(T - T_{\infty}) \tag{2}$$

where

$$T_{\infty} = T_{\rm g} - c_{2\rm g} \tag{3a}$$

$$B = 2.303 c_{1g} c_{2g} \tag{3b}$$

and η^*_∞ is the assumed quasi-universal limiting value for $T \rightarrow \infty$:

$$\eta_{\infty}^* = 10^{-4} - 10^{-3} \,\mathrm{Pa\,s} \tag{4}$$

The apparent activation energy defined in Figure 3 equals

$$E_{\rm a} = R \, {\rm d} \ln \, \eta / {\rm d} (1/T) = R B T^2 / (T - T_{\infty})^2 \qquad (5)$$

If we extrapolate according to this apparent activation energy (as van Krevelen did), we do not find η^*_∞ but



Figure 1 Plot of viscosity η_{cr} vs T_g/T ; for details see text; the dashed part of the curve is an extrapolation

Table 1 Parameters of van Krevelen/Hoftyzer $\eta_{\rm cr}$ correlation^{1,2}. First columns taken from Table 15.5 of ref. 2; $\eta_{\rm cr}(\infty)$ (third column) was calculated with equation (15.38) of ref. 2 (equation (1) of present paper). Subscript cr indicates that the viscosities were taken at the critical molecular weight, M_c , where the *M*-dependence changes from M^{+1} to $M^{3.4}$

Polymer	T _g (K)	$\frac{E_{\eta}(\infty)}{(\text{kJ mol}^{-1})}$	$\frac{10\log \eta_{\rm cr}(\infty)}{\eta \text{ in Pa s}}$
Polyethylene	195	25	-3.53
Polypropylene	253	44	-5.14
Polyisobutylene	198	48	-5.48
Polystyrene	373	59	-6.42
Poly(vinyl chloride)	354	85	-8.63
Poly(vinyl acetate)	301	67	-7.10
Poly(methyl methacrylate)	378	65	-6.93
Poly(butyl methacrylate)	300	72	-7.52
Polybutadiene(cis)	171	26	-3.61
Polyisoprene	220	23	-3.36
Poly(ethylene oxide)	206	27	-3.70
Poly(decamethylene succinate)	210	28	-3.78
Poly(decamethylene adipate)	217	29	-3.87
Poly(decamethylene sebacate)	197	30	-3.95
Poly(ethylene teraphthalate)	343	45	-5.23
Nylon 6	323	36	-4.46
Polycarbonate	414	85	-8.63
Poly(dimethyl siloxane)	150	15	-2.68

viscosity η_{∞} given by (see *Figure 3*)

$$\ln \eta/\eta_{\infty} = E_{\rm a}/[RT] = BT/(T - T_{\infty})^2 \qquad (6)$$

Subtracting equations (2) and (6), we find with equation (5)

$$\ln \eta_{\infty}^*/\eta_{\infty} = BT_{\infty}/[T - T_{\infty}]^2 = E_{\rm a}T_{\infty}/[RT^2] \qquad (7)$$

With equations (3)-(5) and using the quasi-universal WLF parameters (17 and 51), we find:

$$\log \eta_{\infty} - \log \eta_{\infty}^{*} = -[E_{a}/(2.303RT_{\infty})] \\ \times [1 - \sqrt{(RB/E_{a})}]^{2} \\ = -52.2E_{a}[1 - \sqrt{(16.6/E_{a})}]^{2} / \\ \times (T_{g} - 51)$$
(8)

in which E_a is expressed in kJ mol⁻¹. Figure 4 below shows that the η_{∞} predicted with this equation correlates with the limiting viscosity as predicted by van Krevelen's equation. This agreement is not perfect which may be



Figure 2 Limiting viscosity $\eta_{cr}(\infty)$ vs T_g ; data from *Table 1*



Figure 3 On the problems with van Krevelen's extrapolation to $T \to \infty$. We use the abbreviations: $\eta = \eta_{cr}$ and $\eta_{\infty} = \eta_{cr}(\infty)$. For high- T_g polymers, the measurements are done in the region where the line is still curved. This leads to an (apparent) activation energy E_a [defined by equation (5)] higher than the limiting activation energy, $E_\eta(\infty)$, defined (*Figure 1*) for the high-temperature range where the process is really Arrhenius; moreover, the resulting η_{∞} value will be lower than the correct value η_{∞}^* . For low- T_g polymers, the viscosity measurements can be done at temperatures sufficiently above T_g (lower $T_{g/T}$ values); the linear (Arrhenius) part of the line is reached more easily and the limiting values $[E_\eta(\infty) \text{ and } \eta_{\infty}^*]$ are approached better

due to the approximations used (universal WLF constants, a universal value for η_{∞}^* , omission of an additional high-temperature Arrhenius term). Nevertheless, van Krevelen's results are reasonably reproduced and we conclude that the very low limiting viscosities given by van Krevelen and Hoftyzer are not realistic and due to application of an Arrhenius equation in a temperature range where the viscosity is still changing in a



Figure 4 Limiting viscosity η_{∞} calculated with equation (8) from the $T_{\rm g}$ values and activation energies of *Table 1* vs the η_{∞} 's given in the last column of *Table 1* (calculated with equation (1) = equation (15.38) of ref. 2). In equation (8), we used a η_{∞}^* value of 10^{-4} Pa s (same value as for low-molecular weight liquids)

non-Arrhenius way (WLF/Vogel). The limiting values have no direct physical significance; they are merely parameters in some useful correlations¹¹.

Theoretical implications

Linear viscoelastic theory³ gives the general formula

$$\eta = \int_0^\infty G(t) \, \mathrm{d}t \tag{9}$$

where G(t) is the stress-relaxation modulus of the material and η the viscosity at zero strain rate. For low-molecular weight liquids and narrow relaxations (as usual in such liquids at high temperatures), this equation reduces to^{5,6}

$$\eta \approx G_{\rm o} \tau \tag{10}$$

where G_0 is the shear modulus of the rigid (glassy) material and τ the relaxation time.

For organic materials, bounded by secondary forces, the shear modulus is of the order of $1 \text{ GPa}^{9,10}$. The minimum value of τ will correspond to the molecular vibration times, i.e. to about $10^{-14}-10^{-13}$ s. This leads to a limiting viscosity of $10^{-5}-10^{-4}$ Pa s, just as found experimentally⁴⁻⁶. van Krevelen and Hoftyzer's much lower limiting viscosities (down to 10^{-8} Pa s) would completely contradict this generally accepted theoretical picture.

Acknowledgement

The author wishes to thank Dr M. van Gurp for critically reading the manuscript.

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